

Superhydrophobic sodium alginate/cellulose aerogel for the dye adsorption and oil-water separation

Huimin Li

Jiangnan University

Jingyi Huang

Jiangnan University

Chaoran Meng

Jiangnan University

Shen Shen

Jiangnan University

Hongbo Wang

Jiangnan University

Jiajia Fu (✉ kathyfjj@126.com)

Jiangnan University

Research Article

Keywords: Polysaccharide-based aerogel, Hydrophobicity, Dye adsorption, Oil-water separation

Posted Date: October 13th, 2022

DOI: <https://doi.org/10.21203/rs.3.rs-2134219/v1>

License: © ⓘ This work is licensed under a Creative Commons Attribution 4.0 International License.

[Read Full License](#)

1 Superhydrophobic sodium alginate/cellulose aerogel for the dye 2 adsorption and oil-water separation

3 Huimin Li ^{a,b}, Jingyi Huang ^a, Chaoran Meng ^a, Shen Shen ^{a,b}, Hongbo Wang ^{a*}, Jiajia Fu ^{a,b*}

4 ^a Jiangsu Engineering Technology Research Centre for Functional Textiles, Jiangnan University,
5 No.1800 Lihu Avenue, Wuxi, P.R. China

6 ^b China National Textile and Apparel Council Key Laboratory of Natural Dyes, Soochow University,
7 Suzhou 215123, China

8 Abstract

9 The wide application of polysaccharide-based aerogel is limited by its hydrophilicity. To solve this
10 problem, sodium alginate/ sodium carboxymethyl cellulose (SA/CMC) with silica nanoparticles and
11 methyl trimethoxysilane as hydrophobic modifiers was prepared in this study. The sodium alginate (SA)
12 and sodium carboxymethyl cellulose (CMC) were selected because of their low cost and easy of
13 combination with the other two materials. After the silane reagent modification, Ca²⁺ crosslinking,
14 surface plasma treatment, thermochemical vapor deposition and freeze-drying methods, the aerogel get
15 density of 0.080 g/cm³, high porosity of 94%, three-dimensional porous structure with great
16 adsorbed ability. This superhydrophobic SA/CMC aerogel exhibits excellent water stability, appropriate
17 compressive strength and good adsorption capacity of cationic dye methylene blue (MB). And the
18 adsorption process is analyzed by adsorption kinetics. Meanwhile, this aerogel gets great absorbency and
19 efficiency towards varieties of organic solvents, which gives it great potential of being used in the field
20 of oil-water separation, textile dye wastewater treatment, etc. Moreover, this aerogel is expected to be

* Corresponding author; e-mail: kathyfjj@126.com ; wxwanghb@163.com

21 recycled after washing.

22 **Keywords**

23 Polysaccharide-based aerogel; Hydrophobicity; Dye adsorption; Oil-water separation;

24 **Introduction**

25 With the development of the industrialization, organic water pollution (e.g., textile dye wastewater
26 treatment, oil spill, etc) is becoming more and more serious, which caused serious problem to the
27 ecological environment (Lee et al. 2017). Thus, developing novel materials for removing the organic
28 pollutants out of water effectively is of great urgent. And aerogels showed great potential under this
29 circumstances (Zhang et al. 2020). Aerogel is a sort of porous and light-weight materials widely used in
30 the field of catalysis (Niu et al. 2020), adsorption and environmental clean-up (Zhang et al. 2017, Matias
31 et al. 2015, Perdigoto et al. 2012, Guan et al. 2020, Adebajo et al. 2003), acoustic transducers (Long et
32 al. 2021), energy storage devices (Long et al. 2008), thermal isolation (Zheng et al. 2020), flame retardant
33 (Chen et al. 2016), chemical sensors (Plata et al. 2004), and biomedical and pharmaceutical applications
34 (Smirnova et al. 2004, Ulker & Erkey 2014, Yan et al. 2020). Up to our knowledge, the potential
35 application of the aerogel is strongly relied on the materials and microstructure. The microstructure can
36 be controlled during the preparation process, including the sol-gel transition (gelation), network
37 perfection (aging) and gel-aerogel transition (drying) (Zuo et al. 2015). The starting precursors, operating
38 and provision requirements are the decisive factor in a sol-gel reaction of wet chemical synthesis
39 approach to prepare aerogels. Moreover, the generation of the 3D porous network is the most determinant
40 aspect of aerogel fabrication (Maleki 2016, Estella et al. 2007). Although the biodegradable
41 polysaccharide-based aerogels showed great promise in the area of oil-water separation, they are
42 extremely fragile and easy to collapse in water due to the hydrophilicity property of the materials (Fu &

43 Guo 2022, Alvarez-Lorenzo et al. 2013, Reches & Gazit 2003, Autissier et al. 2010, Benbettaieb et al.
44 2016). Therefore, the polysaccharide aerogel without hydrophobic modification, as adsorbent or catalyst,
45 will seriously affect the adsorption effect or catalytic efficiency. It has practical significance to extend
46 and promote the application of the eco-friendly polysaccharide aerogel by changing its hydrophilicity.

47 Alginates and cellulose, both natural polysaccharides that have shown great potential as the most
48 important biocompatible and eco-friendly polymers in nature, which are rich in resources. The
49 evaporation of absorbed water molecules often causes the structure of aerogel to collapse. There are
50 limited its application due to poor mechanical properties and excellent hydrophilicity in the dye
51 adsorption, oil-water separation and recyclability. On the one hand, sodium alginate (SA) can form a 3D
52 network with a unique “egg-box” structure upon ionic crosslinking with divalent cations such as calcium,
53 because the cations cause the G-units on neighboring polysaccharide chains to interact, corresponding to
54 the gels stack that form the structure of the cross-linking network (Jing et al. 2022, Gao et al. 2021, Jeong
55 et al. 2010). Meantime, cellulose derivative aerogels can be prepared by derivatization of cellulose and
56 chemical crosslinking of crosslinking agent (Tan et al. 2001). Sodium carboxymethyl cellulose (CMC),
57 as a solubility polysaccharide with biocompatibility and biodegradation, is a common derivative formed
58 by the carboxymethylation of the hydroxyl group of cellulose (Lin et al. 2016). CMC can easily and
59 quickly cross link with metal ions (such as Ca^{2+} , Mg^{2+} , Al^{3+} and Fe^{3+}) in non-toxic and eco-friendly
60 reaction environment (Lin et al. 2016, Nie et al. 2004, Li et al. 2013, Nadagouda & Varma 2007). On the
61 other hand, the bionic superhydrophobic materials, as a recent research hotspot, are mainly constructed
62 according to the superhydrophobic lotus surface and typical “rose petal” effect in nature (Li et al. 2017).
63 The constructed fabric surfaces with microtemplates for patterning, which are based on the morphology
64 of particles coated on the textile fibre and exhibit an anti-wetting property. Moreover, the

65 superhydrophobic surfaces generally needs the introduction of surface roughness. The hydrophobic
66 interface with hierarchical cellular structure can be achieved by constructing rough micro and nano
67 texturing or introducing low surface energy substances (Li et al. 2017, Wang & Jiang 2007). Hereby, the
68 efficient way of superhydrophobic polysaccharide-based aerogel via silane reagent modification is the
69 most common preparation (Feng et al. 2015). Besides, plasma processing is a kind of modification
70 method with fast etching speed, high uniformity and low pollution in the processing method of
71 microscopic rough structure (Tsougeni et al. 2007). Moreover, the vapour deposition of hydrophobic
72 silanes on sponge-like ultra-porous nanocellulose aerogels can separate the mixed oil and water liquids
73 (Cervin et al. 2012). Xiao et al. developed a superhydrophobic and superelastic graphene oxide/nanofiber
74 aerogel (GNA) after chemical modification and crosslinking via vapor deposition of
75 hexadecyltrimethoxysilane to quickly separate oil-in-water emulsions with an extremely high flux (Xiao
76 et al. 2018). Yang et al. fabricated a robust and superhydrophobic sodium alginate/graphene oxide/silicon
77 oxide aerogel (SA/GO/SiO₂-M) by calcium ion cross-linking self-assembly and chemical vapor
78 deposition, which possesses high efficiency in the separation of surfactant-stabilized water-in-oil
79 emulsions with excellent reusability (Yang et al. 2021).

80 Herein, a superhydrophobic SA/CMC aerogel with silica nanoparticles was fabricated via silane
81 reagent modification, Ca²⁺ crosslinking, surface plasma treatment, thermochemical vapor deposition and
82 freeze-drying methods. The aerogel is explored the adsorption performance and oil-water separation
83 performance for cationic dye methylene blue (MB) and organic solvents. The effect of multi-step process
84 on hydrophobicity was studied in detail through the characterization of selective wettability,
85 adsorbability of various organic solvents, and oil-water separation capability. Meanwhile, the adsorption
86 process of cationic dye MB on the superhydrophobic SA/CMC aerogel was analyzed by the adsorption

87 kinetics analysis. This study shows that the superhydrophobic SA/CMC aerogel are a promising material
88 in treating wastewater pollution from different fields.

89 **2. Materials and methods**

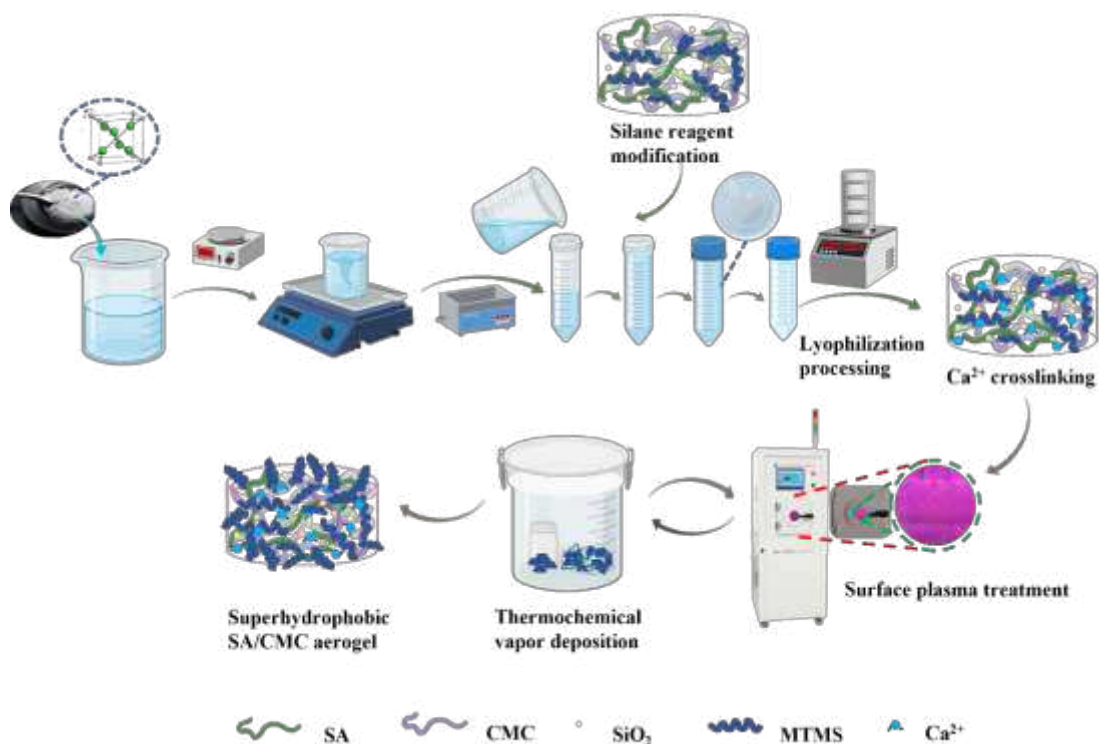
90 **2.1 Materials**

91 Sodium carboxymethyl cellulose (CMC, viscosity: 20 g/L solution, 300–800 mPa · s) and sodium
92 alginate (SA, viscosity: 10 g/L solution, 20°C, ≥ 0.02 Pa · s) were obtained from Sinopharm Chemical
93 Reagent Co., Ltd. (China). Silica (SiO₂) nanoparticles with diameter 15 ± 5 nm and the purity of 99.8
94 wt% was supplied by Shanghai Macklin Biochemical Co., Ltd. (China). Trimethoxymethylsilane
95 (MTMS, purity ≥ 98 wt%), calcium chloride anhydrous (CaCl₂), hexane, anhydrous ethanol (AE) and
96 other chemical reagents were also purchased from Sinopharm Chemical Reagent Co., Ltd. (China).
97 Deionized water (DW) used in the experiments was obtained using an ULUPURE pure water/water
98 system.

99 **2.2 Preparation of the superhydrophobic SA/CMC aerogel**

100 In our present study, we prepared the superhydrophobic SA/CMC aerogel via silane reagent
101 modification, Ca²⁺ crosslinking, surface plasma treatment, thermochemical vapor deposition and freeze-
102 drying methods. SA and CMC were dissolved into 2.0 wt % with optimal stock solutions volume ratios
103 of SA/CMC (m/m) of 1/1 proceeding 2 h at 850 rpm under the condition of agitation at 30 °C. By the
104 way, the freeze-dried sample obtained at this time was distinguished as the SA/CMC aerogel. Briefly, a
105 certain amount of silica nanoparticles (m(SA): m(CMC): m(SiO₂) =10:10:1) was added to the mixture
106 and stirred at 850 rpm for 1 h, and 10 % of the volume fraction of MTMS was also added into the mixture
107 and stirred at 850 rpm for 1 h. Then, the evenly dispersed mixture was sonicated for 30 min before
108 freezing at -80 °C to remove large trapped air bubbles. After freeze-drying, the resulting aerogel was

109 immersed into impregnation solution (m (CaCl₂): m (AE): m (DW) = 2:80:20) for 12 h, and washed with
 110 an excess amount of DW and freeze-dried again. The obtained aerogel was surface modified by low-
 111 temperature plasma treatment in a condition of argon atmosphere for 10 min. Afterward, the aerogel was
 112 obtained in the simple reaction device of cup in cup with MTMS at 80 °C for 4 h. This device of cup in
 113 cup is mainly to prevent direct contact between aerogel sample and MTMS liquid. After fully reaction,
 114 the aerogel was placed in a vacuum drying oven with low pressure to remove the unreacted MTMS.
 115 Finally, the superhydrophobic SA/CMC aerogel was obtained (**Scheme 1, Support Information S1**).



116
 117 **Scheme 1.** Schematic illustration the treatment and possible hydrophobic modification mechanism of the
 118 superhydrophobic SA/CMC aerogel.

119 2.3 Physicochemical Characterizations of the superhydrophobic SA/CMC aerogel

120 The surface morphologies of samples were captured by scanning electron microscope (SEM
 121 SU1510, JPN). The molecular and crystallographic structures of samples were investigated by FT-IR
 122 spectrophotometer (Nicoletis10, USA) using KBr disk method in the range of 4,000–500 cm⁻¹. The

123 crystal-lographic structures of samples were characterized by X-ray diffraction diffractometer (XRD D2
124 PHASER, GER) with a CuK α radiation ($\lambda = 0.15405$ nm) with a scanning rate of 2 min^{-1} at 40 kV and
125 40 mA. The un-treated linen fabric (s0) was also analyzed for comparison.

126 **Measurement for the physical properties of the superhydrophobic SA/CMC aerogel**

127 The thermal stabilities of samples were determined by thermo-gravimetric analyzer (TGA, Q500,
128 USA) with a heating rate of $10 \text{ }^\circ\text{C min}^{-1}$ under N₂ environment from 40 C to 800 $^\circ\text{C}$ as the test
129 temperature range. Stress-strain curves were obtained by Universal Mechanical Materials Tester with
130 loading speed of $10 \text{ mm}\cdot\text{min}^{-1}$ and 80 % of strain is the test end point. Each sample was tested three times
131 to get the average value.

132 **2.4 Density and porosity**

133 The diameter and thickness of samples (circular shape) were measured separately. The density was
134 calculated using the formula (1).

$$135 \quad \rho = \frac{m}{V} \quad (1)$$

136 where m and V are the weight and volume of samples, respectively.

137 The liquid displacement method was used to determine the porosity of samples. The samples (cube,
138 1 cm \times 1 cm \times 1 cm) were put into anhydrous ethanol (AE) to reach a saturation point. All tested samples
139 were gently blotted with filter paper to remove the excess AE and to get the immediately weighed (W).

140 The porosity was calculated using the formula (2).

$$141 \quad P (\%) = \frac{(W-W_0)}{\rho_a V} \times 100\% \quad (2)$$

142 where W_0 and W are the weight of samples before and after being immersed in AE, respectively; V is
143 the sample volume before immersion and ρ_a is the density of alcohol.

144 **2.5 Measurement of water stability for the superhydrophobic SA/CMC aerogel**

145 The water contact angles (WCAs) were measured at room temperature and ambient relative
146 humidity using a DSA25 contact angle analyzer connected to drop shape analysis software. The water
147 contact angles for each sample were measured more than five times on the SA/CMC aerogel and the
148 superhydrophobic SA/CMC aerogel. The water stability of the prepared aerogel in the water was also
149 investigated (**Support Information S2**).

150 **2.6 Dye adsorption performance test**

151 Methylene blue trihydrate ($C_{16}H_{18}ClN_3S \cdot 3H_2O$) (Kannan & Sundaram 2001) was dissolved in
152 various concentrations (0.6 mg/L 0.8 mg/L 1.0 mg/L 2.0 mg/L 4.0 mg/L), which were used as MB
153 standard solutions of the concentration required by the experiment. DW was used as control group and
154 measurement baseline. Then the standard concentration gradient of MB solution of samples was
155 determined spectrophotometrically at 664 nm following the Bouguer-Beer-Lambert Law (Mayerhofer et
156 al. 2020). The concentration of residual dye in different MB solution was measured after equal-weight
157 samples reached the adsorption equilibrium in 50 mL centrifuge tube at 200 rpm. The removal percentage
158 and adsorption value of MB were calculated using the formula (3)(4)(5).

$$159 \quad R_e (\%) = \frac{C_0 - C_e}{C_0} \times 100\% \quad (3)$$

$$160 \quad Q_e = \frac{(C_0 - C_e)V_d \times N}{m_0} \quad (4)$$

$$161 \quad Q_t = \frac{(C_0 - C_t)V_d \times N}{m_0} \quad (5)$$

162 where R_e (%), Q_e and Q_t (mg/g) are dye removal percentage, dye adsorption capacity at equilibrium and
163 t moment, respectively; C_0 , C_e and C_t (mg/L) are the dye concentration at initial, equilibrium and t
164 moment, respectively; V_d (L) is the volume of the dye solution; m_f (g) is the initial mass of the aerogel;
165 N is dilution ratio.

166 **2.7 The adsorption kinetics of the superhydrophobic SA/CMC aerogel**

167 The pseudo-second-order model and intra-particle diffusion can be used to explore the adsorption
168 rate and behavior of pollutants on aerogel for studying its adsorption kinetics (Vimonses et al. 2009, Ho
169 & McKay 1999). The pseudo-second-order model can be used to judge the adsorption properties of
170 aerogel, which were calculated using the formula (6).

$$171 \quad \frac{t}{Q_t} = \frac{1}{K_2 Q_e^2} + \frac{t}{Q_e} \quad (6)$$

172 Where Q_e , Q_t ($\text{mg}\cdot\text{g}^{-1}$) are the adsorption capacity at equilibrium and t moment, respectively. K_2 ($\text{mg}\cdot\text{g}^{-1}$
173 $\cdot\text{min}^{-1}$) is the pseudo-second-order model rate constant and t (min) is adsorption time.

174 The adsorption rate of adsorbents on porous material is usually controlled by the transfer rate at the
175 solid-liquid interface or inside the particle. The intra-particle diffusion within the particle is often used
176 to evaluate the diffusion mechanism of the adsorption process, which were calculated using the formula
177 (7).

$$178 \quad Q_t = K_{id} t^{1/2} + C_{id} \quad (7)$$

179 Where K_{id} ($\text{mg}\cdot\text{g}^{-1}\cdot\text{min}^{-1/2}$) is diffusion rate constant of the intra-particle diffusion. The larger the
180 diffusion rate constant is, the easier the adsorbent diffuses inside the adsorbent. C_{id} is a constant involving
181 the boundary molecular layer including thickness and boundary layer. A linear line with slope K_{id} and
182 intercept C_{id} can be obtained by drawing $t^{1/2}$ and Q_t . The adsorption process is controlled by a single rate
183 of intra-particle diffusion if the line passes through the origin. Otherwise, the adsorption process is
184 controlled by both intra-particle and interfacial diffusion (Kannan & Sundaram 2001).

185 **2.8 Adsorption performance test of simulated organic pollutants**

186 In order to test the adsorption performance of the superhydrophobic SA/CMC aerogel on organic
187 pollutants, such as hexane, chloroform, oil pumping, AE, toluene and paraffin liquid were selected as the
188 adsorbent of organic solvents. And the adsorption capacity and adsorption rate of prepared aerogel were

189 measured respectively to evaluate the adsorption performance of the prepared aerogel. Samples of the
190 same weight were put into 35 mL of various organic solvents to reach adsorption equilibrium at room
191 temperature, then removed from various organic solvents. All tested samples needed gently blotted with
192 filter paper to remove the excess various organic solvents and got the immediately weighed. Each sample
193 was tested three times to get the average value. The adsorption performance was calculated using the
194 formula (8)(9).

$$195 \quad M_{oil/org} = \frac{m_s - m_0}{m_0} \quad (8)$$

$$196 \quad V_{oil/org} = \frac{\rho}{\rho_{oil/org}} \times \frac{m_s - m_0}{m_0} \quad (9)$$

197 where $M_{oil/org}$ (g/g) is mass adsorption capacity ratio; $V_{oil/org}$ (cm³/cm³) is the volume adsorption capacity
198 ratio; m_s and m_0 (g) are the weight of samples before and after being immersed in various organic solvents;
199 ρ and $\rho_{oil/org}$ (g/cm³) are the density of aerogel and various organic solvents, respectively.

200 **2.9 Oil-water separation experiment**

201 Hexane and chloroform were selected as two kinds of oils and organic solvents with opposite density
202 compared with water. Chloroform ($\rho_{chloroform} > \rho_{water}$) and hexane ($\rho_{hexane} < \rho_{water}$) were dyed red with sudan
203 red G and DW blue with methylene blue. The oil-water separation performance of the superhydrophobic
204 SA/CMC aerogel (circular shape, diameter: 15 mm \pm 0.1mm, thickness: 3 mm \pm 0.1mm) was
205 quantitatively characterized by filtration with 10 mL syringe. Chloroform, hexane and DW were mixed
206 at a 1:1 volume ratio to form 4 mL oil-water mixture, which poured into the 10 mL syringe
207 containing aerogel. Meanwhile, the glass bottle was placed under the syringe hole as a liquid collection
208 device to conduct oil-water separation test and observe the effect. The separation efficiency is
209 characterized by the volume ratio or mass ratio of the liquid collected before and after separation. The
210 separation efficiency is calculated by measuring the mass of the liquid before and after separation using

211 the formula (10):

$$212 \quad \eta(\%) = \frac{m_b}{m_a} \times 100\% \quad (10)$$

213 where η (%) is the separation efficiency; m_a and m_b (g) are the mass of oil before and after filtration,
214 respectively.

215 The oil-water separation flow rate of aerogel can be expressed by the fluid flux of aerogel (F), which
216 is an important index to measure the oil-water separation performance of aerogel and can be obtained by
217 the following formula (11):

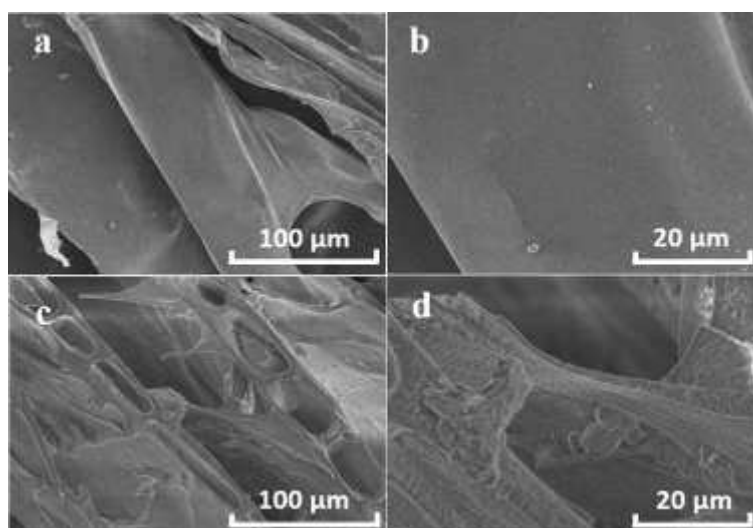
$$218 \quad F = \frac{V}{A} \times \Delta t \quad (11)$$

219 Where F is the fluid flux of aerogel; V (mm³) is the volume of filtrate collected after separation
220 experiment through aerogel; A (mm²) is the effective filtration area of separation experiment; Δt (s) is
221 the time required for the whole oil-water separation experiment to pass through the aerogel.

222 **3 Results and Discussion**

223 **3.1. Characterization of the superhydrophobic SA/CMC aerogel**

224 The morphology is a vital feature for various samples. **Fig.1** shows the microstructure of the
225 SA/CMC aerogel and the superhydrophobic SA/CMC aerogel. The surface of the SA/CMC aerogel is
226 smooth and flat, and the pore structure is not obvious and irregular with small cracks locally. After
227 hydrophobic modification, the morphological changes of the superhydrophobic SA/CMC aerogel are
228 obviously observed. The porous structure presents an increasingly pronounced pore in size of 20 μm with
229 rough surface.

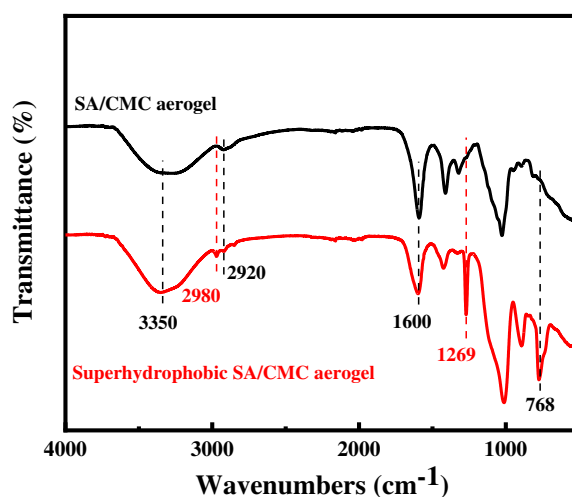


230

231 **Fig. 1.** Scanning electron microscope (SEM) images of **(a, b)** the SA/CMC aerogel and its high
 232 magnification, **(c, d)** the superhydrophobic SA/CMC aerogel and its high magnification.

233

234 The FTIR spectra of the SA/CMC aerogel and the superhydrophobic SA/CMC aerogel are compared
 235 in **Fig. 2.** The bands of SA at 1600 cm^{-1} are attributed to asymmetric stretching vibrations of COO^- (Jiao
 236 et al. 2016). The absorption peaks at 1600 cm^{-1} and 2920 cm^{-1} are found in all spectra, which are mainly
 237 ascribed to the carbonyl group (C=O), and the C-H bond on the molecular chain of SA and CMC,
 238 respectively. The characteristic peaks at 3350 cm^{-1} in all spectra are ascribed to O-H on SA and CMC.
 239 The superhydrophobic SA/CMC aerogel showed several new absorption peaks at 1269 and 768 cm^{-1}
 240 appeared due to Si-O and Si-O-Si bonds in silicane, respectively. The characteristic peaks at 2980 cm^{-1}
 241 corresponded to the vibrations of CH_3 bond (Robb et al. 2002) (Zhou et al. 2018, Zhou et al. 2015). In
 242 addition, C-O stretching vibration absorption peaks at $1100\text{--}1000\text{ cm}^{-1}$ are slightly strengthened, which
 243 is probably due to the coincidence of Si-O-Si absorption peaks. These indicate that MTMS successfully
 244 modified the superhydrophobic SA/CMC aerogel and formed covalent bond with hydroxyl group
 245 through dehydration condensation.



246
247 **Fig. 2.** FT-IR spectra of the SA/CMC aerogel and the superhydrophobic SA/CMC aerogel.

248

249 The crystalline structures of the SA/CMC aerogel and the superhydrophobic SA/CMC aerogel were

250 determined by X-ray diffraction patterns. Obviously, **Fig. 3** exhibits the SA/CMC aerogel has the higher

251 crystallinity than the superhydrophobic SA/CMC aerogel. There are two distinct characteristic diffraction

252 peaks at $2\theta = 10.2^\circ$ and $2\theta = 21.5^\circ$ in the SA/CMC aerogel, while there is not obvious diffraction peak in

253 the superhydrophobic SA/CMC aerogel. The main reason is that the adding of SiO₂ nanoparticles and

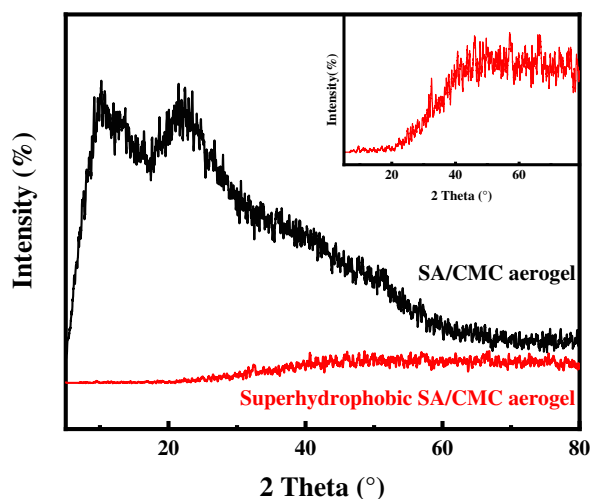
254 trimethoxymethylsilane and subsequent hydrophobic modification disrupt the arrangement of polymer

255 crystals and form irregular and amorphous regions leading to the low crystallinity of superhydrophobic

256 SA/CMC aerogel (Abhari et al. 2017). It ensured the uniform mixing of them and prevented the

257 crystallization behavior of the SA/CMC aerogel. Thus the amorphous composite superhydrophobic

258 SA/CMC aerogel formed (Chang et al. 2009).



259

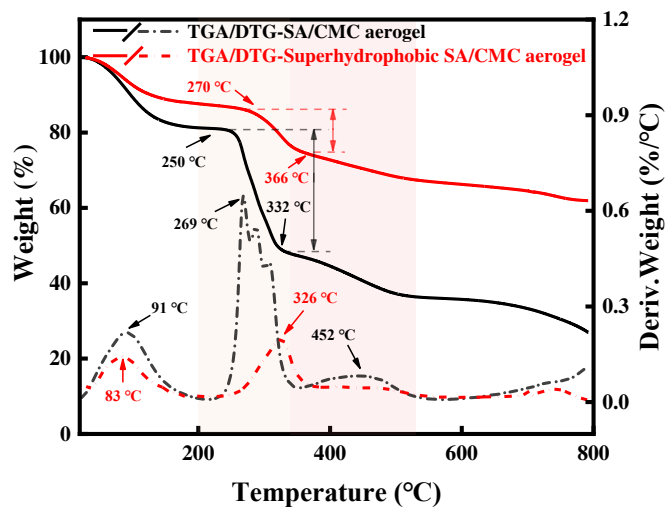
260 **Fig. 3.** X-ray diffraction pattern of the SA/CMC aerogel and the superhydrophobic SA/CMC aerogel.

261

262 3.2 The thermal stability of the superhydrophobic SA/CMC aerogel

263 The thermo-stabilities of the SA/CMC aerogel and the superhydrophobic SA/CMC aerogel were
 264 evaluated by the thermogravimetry analysis (TGA) and differential thermogravimetry (DTG). As shown
 265 in **Fig. 4**, the two kinds of aerogels exhibit four steps of active weight loss with elevating temperature.
 266 The rapid weight loss below 100 °C was attributed to the release of moisture from the aerogels. In the
 267 dehydration stage, the weight loss rate of the SA/CMC aerogel and the superhydrophobic SA/CMC
 268 aerogel reached about 19% and 13 %, respectively. The main reason is that the escape of adsorbed water
 269 on the surface and internal pores of aerogels during evaporation. It is speculated that the reason for the
 270 difference is that the internal and surface structures of the two kinds of aerogels are significantly different
 271 with pore sizes and adsorbed moisture content. On the other hand, the differences in hygroscopicity of
 272 aerogels are reflected the hydrophobic modification can significantly reduce the hygroscopicity of
 273 aerogel. In addition, the initial thermal decomposition temperature of aerogels ranges from 200°C to
 274 350°C. The polysaccharide base polymer network structure begins to depolymerize and the chain

275 structure breaks, resulting in a very significant weight loss region of aerogel at this stage (Abhari et al.
276 2017, Liang & Hirabayashi 1992). The mass loss rates of aerogel and hydrophobic aerogel were as high
277 as 34% and 12%, respectively, which showed significant differences. Then, the aerogels slowly loses
278 weight with the increase of temperature from 350°C to 540°C, suggesting that the components in aerogels
279 are further thermologically decomposed. Moreover, the weight loss rate of the superhydrophobic
280 SA/CMC aerogel is always smaller than that of the SA/CMC aerogel. In addition, the temperature higher
281 than 540°C is the carbonization stage of aerogel. With the increase of temperature, the trend of weight
282 loss rate curve of aerogels shows that polysaccharides and other components are completely thermal
283 degraded to form carbon oxides, and finally become inorganic components. The initial decomposition
284 temperature of the superhydrophobic SA/CMC aerogel increased from 250 °C of the SA/CMC aerogel
285 to 270 °C, and the maximum decomposition temperature also increased from 269 °C of the SA/CMC
286 aerogel to 326 °C. It indicated that the reduction in crystallinity after hydrophobic modification has little
287 effect on the increase of the thermal stability of the superhydrophobic SA/CMC aerogel. Besides,
288 Ca²⁺ crosslinking can form a 3D network with a unique “egg-box” structure upon ionic crosslinking. SA
289 and CMC produce strong chemical bonds with MTMS and Ca²⁺ leading to a tighter and more solid
290 structure. Thus, the relatively high thermal stability appeared in superhydrophobic SA/CMC aerogel.



291

292 **Fig. 4.** Thermogravimetric analysis of the SA/CMC aerogel and the superhydrophobic SA/CMC aerogel

293 about TGA curves and DTG curves.

294 3.3. Functionalities of the superhydrophobic SA/CMC aerogel

295 The porosities of the aerogels are decreasing with the increase of polysaccharide concentration in

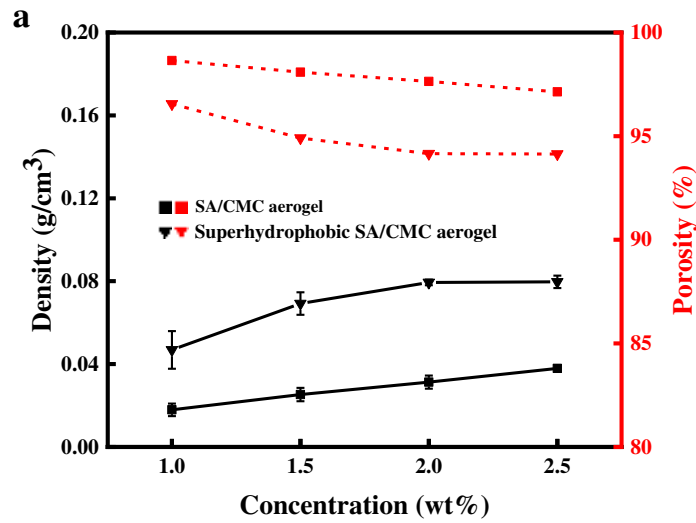
296 **Fig 5a.** This trend is contrary to the density of the aerogels curve. The porosities of the SA/CMC aerogel

297 and the superhydrophobic SA/CMC aerogel are 97.64% and 94.16%, respectively. The densities of the

298 SA/CMC aerogel and the superhydrophobic SA/CMC aerogel are 0.03129 and 0.0794 g/cm³,

299 respectively. **Fig 5b** indicating the superhydrophobic SA/CMC aerogel can stand on the top of flower

300 stamens and dried flower because it's light enough.



301



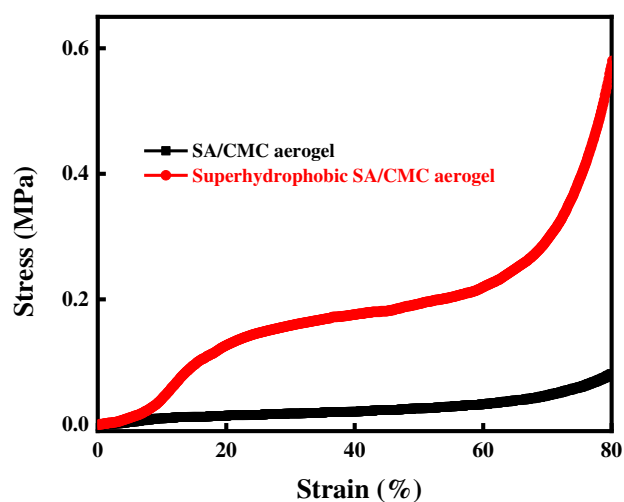
302

303 **Fig.5. (a)** Density and porosity of the SA/CMC aerogel and the superhydrophobic SA/CMC aerogel with
 304 various concentration. Data are mean \pm SD (n = 3); **(b)** Optical images indicating the superhydrophobic
 305 SA/CMC aerogel can stand on the top of flower stamens and dried flower.

306

307 The perfect skeleton structure of aerogel can enhance its mechanical strength. Moreover, it plays an
 308 important role in the process of oil adsorption and storage and oil-water separation. The compressive
 309 stress-strain curves for the SA/CMC aerogel and the superhydrophobic SA/CMC aerogel are exhibited
 310 in **Fig. 6**. The aerogels show different curves, indicating that the addition of SiO₂ nanoparticles and
 311 hydrophobic modification influence the mechanical property of the SA/CMC aerogel. The
 312 superhydrophobic SA/CMC aerogel could be compressed to more than 80% without mechanical failure
 313 due to the flexibility of CMC and SA with Ca²⁺ crosslinking. The appropriate compressive stress would

314 be beneficial to the integrity maintenance in practical applications (Zhou et al. 2018).



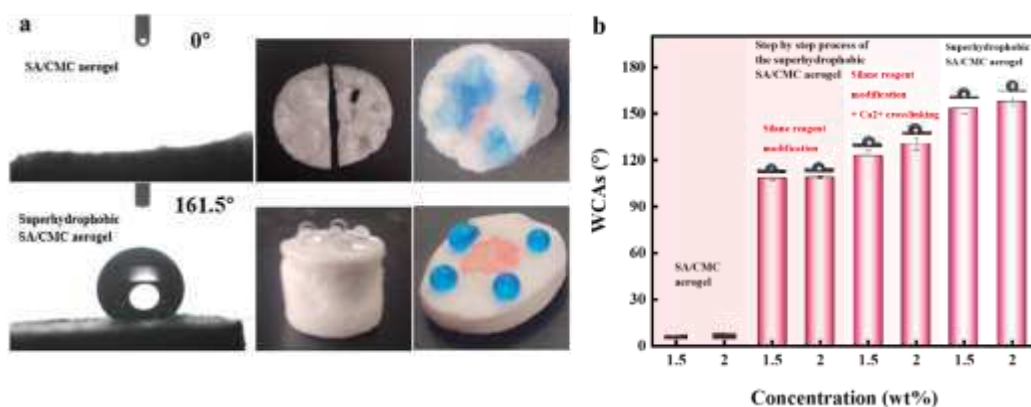
315

316 **Fig.6.** Compressive stress-strain curves of the SA/CMC aerogel and the superhydrophobic SA/CMC
317 aerogel with strain of 80%.

318

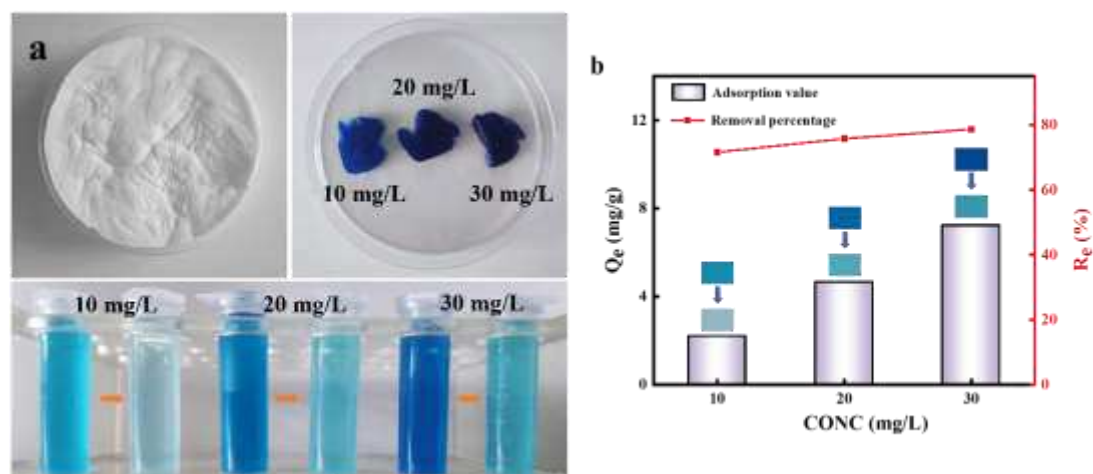
319 The effect of each step in the hydrophobic modification process on the water stability of aerogels is
320 shown in **Support Information S2**. Benefiting from the high surface roughness and polysaccharide
321 matrix with porous structure, the superhydrophobic SA/CMC aerogel shows superhydrophobicity and
322 superoleophilicity (Zhou et al. 2018). The WCAs for aerogels are exhibited in **Fig. 7**. As expected, the
323 superhydrophobic SA/CMC aerogel was hydrophobic with a WCA of 161.5°, which could be ascribed
324 to adding silica nanoparticles and successful silanizing modification. **Fig. 7a** exhibits the aerogel could
325 leave the water droplets standing on its surface, while absorbing the chloroform droplet. As shown in
326 **Fig. 7b** and **Support Information S3**, the water contact angles (WCAs, °) of SA/CMC aerogel with
327 various concentration are 0°. All the hydrophobic modification steps promoted the hydrophobic
328 properties of aerogels. A remarkable increase of WCA up to 161.5° was achieved with a series of
329 hydrophobic modifications, demonstrating the superhydrophobicity of the obtained composite aerogels.

330 The hydrophobic properties of aerogels could be improved by increasing the concentration of
 331 polysaccharide and silane reagent in the same proportion. A preliminary hydrophobic modification
 332 process of silanization could be carried out in the sol-gel reaction process to improve the hydrophobicity
 333 of the SA/CMC aerogel. The obtained aerogel with preliminary hydrophobic modification using silane
 334 reagent has more stable structure and better performance after Ca²⁺ crosslinking. Further, surface plasma
 335 treatment prompts the hydroxyl functional groups on SA and CMC on the surface of the aerogel can be
 336 activated and exposed, which is conducive to thermochemical vapor deposition as the subsequent
 337 hydrophobic modification of silanization. Besides, the water droplet would return to its original shape
 338 immediately after leaving the surface of the aerogel. The resultant figures present that the
 339 superhydrophobic and superoleophilic SA/CMC aerogel with good hydrophobicity and low water
 340 adhesion ensured that the oil agent could permeate and move through it, which is good for the oil-water
 341 separation performance.



342
 343 **Fig.7. (a)** Optical images of the process of water contacting the surface of two kinds of aerogels and
 344 water (blue) and chloroform (red) on the surface of them; **(b)**The water contact angles (WCAs, °) of the
 345 SA/CMC aerogel and the superhydrophobic SA/CMC aerogel with two kinds of polysaccharide
 346 concentrations in different processing stages when the water drops stabilized after falling (0.25 s). Data
 347 are mean ± SD (n = 3).

348 Methylene blue (MB, $C_{16}H_{18}ClN_3S$) is a widely used cationic dye, which can be selected as the
349 target dye pollutant (Kannan & Sundaram 2001). The superhydrophobic SA/CMC aerogel could be used
350 to adsorb the MB, and its equilibrium adsorption capacity increases with initial concentration. **Support**
351 **Information S4** exhibits the correlation between the concentration of MB and its absorbance. As shown
352 in **Fig. 8**, under the three different initial concentrations of MB, the equilibrium adsorption capacities of
353 the superhydrophobic SA/CMC aerogel are 2.19 mg/g, 4.64 mg/g and 7.22 mg/g, and the dye removal
354 percentage are 71.59 %, 75.79 % and 78.63 %, respectively. The main reason is the electrostatic attraction
355 as the main force between aerogel and MB.

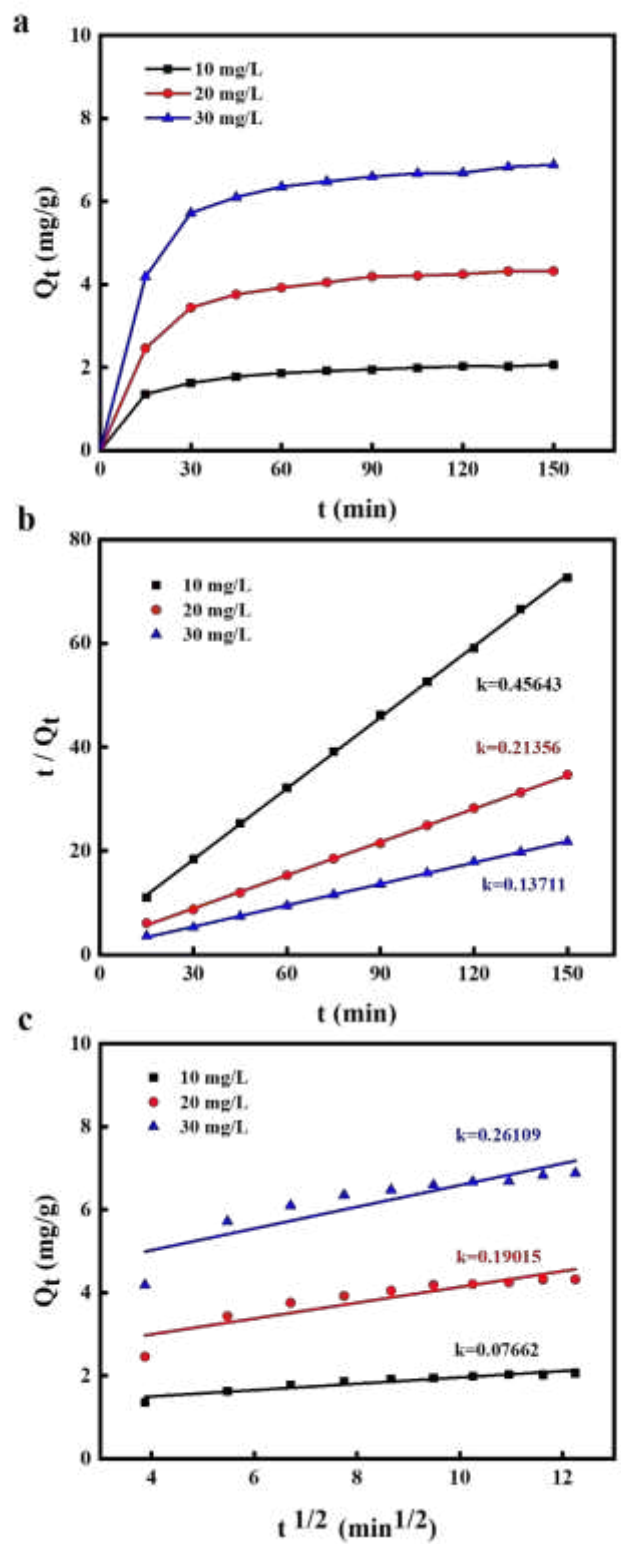


356
357 **Fig.8.** Optical images of the superhydrophobic SA/CMC aerogel and MB solution concentration changes
358 (a) before and (b, c) after adsorption. (d) MB removal percentage and equilibrium adsorption capacity
359 at different initial concentrations of MB.

360

361 According to the **Fig. 9** and **Table 1**, it can be seen the R_2^2 is greater than 0.999 that very close to
362 1, indicating that the experimental data are highly consistent with the curve fitted by the pseudo-second-
363 order model. The value of Q_{ec2} is highly close to the Q_{ee} obtained from the actual experiment. Above all
364 can show that the superhydrophobic SA/CMC aerogel of MB adsorption dynamics behavior conforms to

365 the pseudo-second-order model. The adsorption rate of MB by the superhydrophobic SA/CMC aerogel
366 is linearly related to the mass of aerogel and the initial concentration of MB. The adsorption process is
367 mainly chemical adsorption, which is closely related to the chemical composition of aerogel. The process
368 of MB adsorption by the superhydrophobic SA/CMC aerogel could also be directly fitted to a continuous
369 curve with linear relationship by the intra-particle diffusion. The straight line that passes through the
370 origin and above it, indicating that the kinetic process of MB adsorption by aerogel is affected by both
371 intra particle diffusion and boundary layer diffusion. As depicted in **Fig.9c**, the boundary molecular layer
372 constant C_{id} as the intercept of the line is greater than 0, indicating that there is a rapid adsorption process
373 in the process of MB adsorption, where the slope of the line represents the diffusion rate constant in the
374 particle (Wu et al. 2009). Moreover, the higher the initial concentration of MB was, the lower the degree
375 of linear fit of the model became. Therefore, the adsorption process can be further refined into three
376 stages. The first stage is the surface adsorption stage within 30 min. The adsorption rate is the fastest and
377 the intra-particle diffusion rate is the largest. The main reason is that the high initial concentration of MB
378 and the high porosity of aerogel can quickly adsorb a large number of dye molecules in the solution. The
379 second stage mainly occurred the adsorption rate gradually slows down in the 30-90 min period. The dye
380 molecules gathered on the outer surface of aerogel would increase with time, and MB would diffuse in
381 the small pores inside aerogel. The third stage occurs after 90 min of adsorption. There are fewer dye
382 molecules in the solution. The active adsorption sites on aerogel surface decreased with the decrease of
383 MB concentration. Therefore, the adsorption rate is the slowest and the diffusion rate in particles is the
384 smallest at this stage. Finally, the adsorption equilibrium state will be reached.



385

386 **Fig.9.** The influence of time on adsorption of MB with different initial concentrations by the
 387 superhydrophobic SA/CMC aerogel and the fitting curves of adsorption kinetics **(a)**; fitting curve of
 388 pseudo-second-order model **(b)**; fitting curve of intra-particle diffusion **(c)**.

389 **Table 1.** The adsorption kinetics parameters of the superhydrophobic SA/CMC aerogel for MB solutions
 390 with different initial concentrations

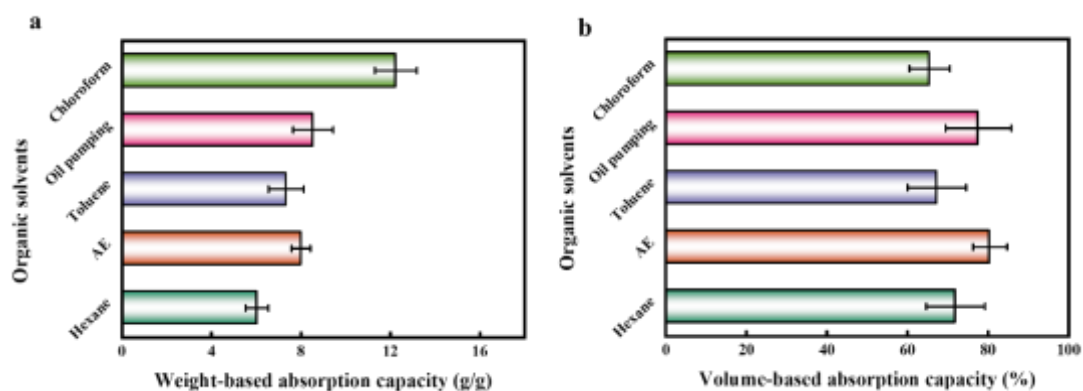
Kinetic model	C_0 (mg/L)	K_2 (g/mg min)	Q_{ec2} (mg/g)	R_2^2
Pseudo-second-order	10	0.044649	2.190916	0.99977
	20	0.018212	4.682525	0.99963
	30	0.014491	7.293414	0.99959
Kinetic model	C_0 (mg/L)	K_{id} (mg/g min ^{1/2})	C_{id} (mg/g)	R_3^2
Intra-particle diffusion	10	0.07662	1.19477	0.9054
	20	0.19015	2.23771	0.82331
	30	0.26109	3.97997	0.76405

391

392 The superhydrophobic SA/CMC aerogel is an ideal candidate for the sorption of organic pollutants
 393 due to its high porosity, compressive stability and hydrophobicity. The superhydrophobic SA/CMC
 394 aerogel has a certain weight and volume adsorption capacity for various oils and organic solvents are
 395 6–12 g/g and 65%–80% in **Fig. 10**. It exhibits the oil droplet could be absorbed by the aerogel
 396 immediately when it contacted the aerogel surface. The superhydrophobic SA/CMC aerogel
 397 preferentially adsorbs to a layer of oils and organic solvents dyed red in the oil-water mixture, such as
 398 paraffin liquid, chloroform and hexane. In particular, chloroform has the best effect in the selective
 399 competitive adsorption process of the superhydrophobic SA/CMC aerogel in **Support Information S5**.
 400 Chloroform ($\rho_{\text{chloroform}} > \rho_{\text{water}}$, red) and hexane ($\rho_{\text{hexane}} < \rho_{\text{water}}$, red) were selected as two kinds of oils and
 401 organic solvents with opposite density compared with water (blue). In order to further demonstrate the
 402 absorbing capability of the superhydrophobic SA/CMC aerogel in oil-water separation, various kinds of

403 organic solvents (e.g., chloroform and hexane etc.) were tested by a simple device in **Fig.11**. The oil/water
 404 mixture can be separated by gravity. The organic solvents could slowly permeate the aerogel and the
 405 water is remains on top of the aerogel in the syringe. The separation efficiency of chloroform is 58.27%
 406 and the fluid flux of oil-water separation is 74.66 mm·s. The aerogel will form an oil layer in the lower
 407 layer because it has a certain adsorption effect on the oil, which prevents the further penetration of water
 408 to successfully realize the separation of the oil-water mixture. Moreover, the superhydrophobic SA/CMC
 409 aerogel has a good separation effect on oil-water mixture retaining original structure after adsorption.
 410 However, the separation effect of this filtration method is not good for oil with density less than water
 411 (**Fig.11b**). The main reason is that the oil contacted with the aerogel can percolate down to be collected
 412 in the bottle. But the oil that has been blocked by the water layer from contacting the aerogel eventually
 413 unable to be filtered by gravity when the oil-water mixture is poured. The superhydrophobic SA/CMC
 414 aerogel after adsorbing organic liquids could be recycled by mechanically squeezing out oils or drying
 415 absorbed samples at above the boiling point, which avoids the pollution and realizes the recyclability of
 416 organic solvents further.

417

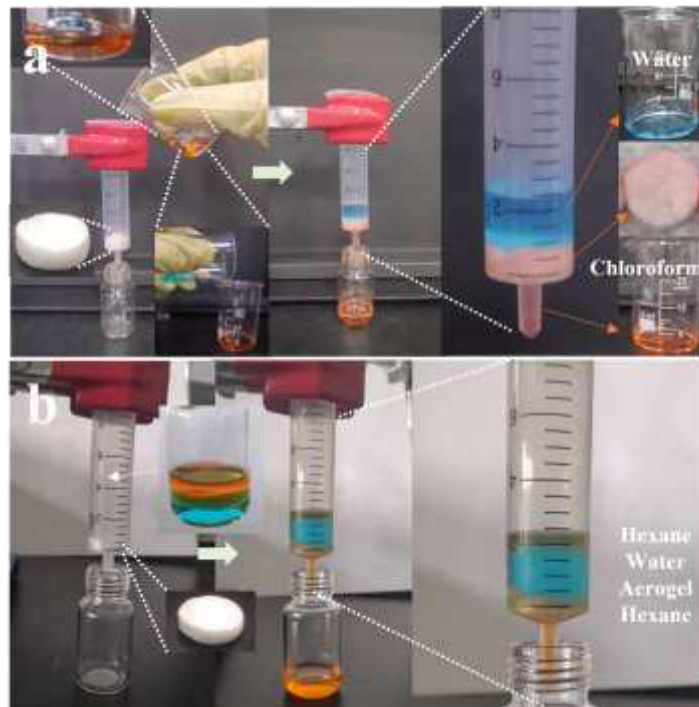


418

419 **Fig.10.** (a) Mass and (b) volumetric adsorption capacity of the superhydrophobic SA/CMC aerogel for

420 different oils and organic solvents ($\rho_{\text{chloroform}}=1.484 \text{ g/cm}^3$, $\rho_{\text{oil pumping}}=0.874 \text{ g/cm}^3$, $\rho_{\text{toluene}}=0.866 \text{ g/cm}^3$,

421 $\rho_{AE}=0.7893 \text{ g/cm}^3$, $\rho_{\text{hexane}}=0.6594 \text{ g/cm}^3$).



422

423 **Fig.11 (a, b)** Schematic diagram of oil-water mixture separation process.

424 **Table 2.** Separation effect of the superhydrophobic SA/CMC aerogel for chloroform /water mixture

Test	m_a/g	m_b/g	V/mm^3	A/mm^2	$\Delta t/s$	$\eta/\%$	F
1	2.9832	1.8545	1243.296	176.7146	10.03	62.16	70.57
2	2.9832	1.5304	1026.012	176.7146	12.61	51.30	73.21
3	2.9832	1.8302	1227.005	176.7146	11.55	61.35	80.20
Average	2.9832	1.7384	1165.438	176.7146	11.40	58.27	74.66

425

426 **4 Conclusion**

427 In this study, the superhydrophobic SA/CMC aerogel was successfully fabricated and demonstrated

428 the feasibility of an effective absorbent for targeting dye methylene blue (MB) and organic pollutants.

429 The advantages of aerogel also include a green preparation environment, and a mild modification method,

430 including silane reagent modification, Ca²⁺ crosslinking, surface plasma treatment, thermochemical
431 vapor deposition and freeze-drying methods. The obtained aerogel represented superior physical features,
432 including low density, high porosity, mechanical stability, superhydrophobicity, water stability and
433 stable adsorption capacity for dyes and organic solvents. Furthermore, it is found that the initial MB
434 concentration significantly affects the absorption capability of the aerogel. The pseudo-second-order
435 model and intra-particle diffusion are applied to describe and validate the MB absorption behavior of the
436 aerogel. Moreover, it could separate oil-water mixture without external pressure for various organic
437 solvents. Consequently, the superhydrophobic SA/CMC aerogel offers a great feasibility for various
438 applications in the fields of environment remediation, organic solvents purification and removal of
439 organic liquids from waterbody etc.

440 **Declarations**

441 **Conflict of interest**

442 The authors declare that they have no known competing financial interests or personal relationships
443 that could have appeared to influence the work reported in this paper.

444 **Funding / Acknowledgments**

445 We gratefully acknowledge the Support by the Opening Project of China National Textile and
446 Apparel Council Key Laboratory of Natural Dyes, Soochow University (No.SDHY2122), the National
447 Natural Science Foundation of China (No.31470509) and Jiangsu Natural Science Foundation for
448 General project (BK20191199).

449 **Author Contribution**

450 CRediT authorship contribution statement

451 Huiming Li: Conceptualization, Investigation, Data curation, Writing - original draft. Jingyi Huang:
452 materials preparation. Chaoran Meng and Shen Shen: review & editing. Hongbo Wang and Jiajia Fu:
453 review & editing; Supervision & Funding acquisition. All authors reviewed the manuscript.

454 **Ethics approval and consent to participate**

455 Not applicable

456 **Consent for publication**

457 All authors believe that the findings of this study are relevant to the scope of your journal and will be of
458 interest to its readership.

459 **Availability of data and materials**

460 The results/data/figures in this manuscript have not been published elsewhere, nor are they under
461 consideration (from all authors) by another publisher.

462 **Authors' information (optional)**

463 Huimin Li

464 Jiangnan University

465 1800 Lihu Avenue, Wuxi 214122, China

466 Tel: 0086-15764233420

467 Email Address: 7200707007@stu.jiangnan.edu.cn

468

469 Jingyi Huang

470 Jiangnan University
471 1800 Lihu Avenue, Wuxi 214122, China
472 Email Address: hjy364570266@163.com
473
474 Chaoran Meng
475 Jiangnan University
476 1800 Lihu Avenue, Wuxi 214122, China
477 Email Address: 8202101470@jiangnan.edu.cn
478
479 Shen shen
480 Jiangnan University
481 1800 Lihu Avenue, Wuxi 214122, China
482 Email Address: 7170707009@stu.jiangnan.edu.cn
483
484 Hongbo Wang
485 Jiangnan University
486 1800 Lihu Avenue, Wuxi 214122, China
487 Email Address: wxwanghb@163.com
488
489 Jiajia Fu
490 Jiangnan University
491 1800 Lihu Avenue, Wuxi 214122, China
492 Email Address: kathyfjj@126.com

493 **References**

494 C. H. Lee, B. Tiwari, D. Zhang, Y. K. Yap (2017) Water purification: oil–water separation by
495 nanotechnology and environmental concerns. *Environ Sci-Nano* 4: 514-525.

496 <https://doi.org/10.1039/c6en00505e>

497 N. Zhang, Y. F. Qi, Y. N. Zhang, J. L. Luo, P. Cui, W. Jiang (2020) A Review on Oil/Water Mixture
498 Separation Material. *Ind Eng Chem Res* 59: 14546-14568.

499 T. T. Niu, B. Zhou, Z. H. Zhang, X. J. Ji, J. M. Yang, Y. H. Xie, . . . A. Du (2020) Low-Temperature
500 Synthesis of Monolithic Titanium Carbide/Carbon Composite Aerogel. *Nanomaterials* 10.

501 <https://doi.org/10.3390/nano10122527>

502 C. Z. Zhang, C. Dai, H. Q. Zhang, S. T. Peng, X. Wei, Y. D. Hu (2017) Regeneration of mesoporous silica
503 aerogel for hydrocarbon adsorption and recovery. *Mar Pollut Bull* 122: 129-138.

504 <https://doi.org/10.1016/j.marpolbul.2017.06.036>

505 T. Matias, J. Marques, M. J. Quina, L. Gando-Ferreira, A. J. M. Valente, A. Portugal, L. Duraes (2015)
506 Silica-based aerogels as adsorbents for phenol-derivative compounds. *Colloid Surface* 480: 260-269.

507 <https://doi.org/10.1016/j.colsurfa.2015.01.074>

508 M. L. N. Perdigoto, R. C. Martins, N. Rocha, M. J. Quina, L. Gando-Ferreira, R. Patricio, L. Duraes
509 (2012) Application of hydrophobic silica based aerogels and xerogels for removal of toxic organic

510 compounds from aqueous solutions. *J Colloid Interface Sci* 380: 134-140.

511 <https://doi.org/10.1016/j.jcis.2012.04.062>

512 Y. Guan, J. Rao, Y. L. Wu, H. Gao, S. Q. Liu, G. G. Chen, F. Peng (2020) Hemicelluloses-based magnetic
513 aerogel as an efficient adsorbent for Congo red. *Int J Biol Macromol* 155: 369-375.

514 <https://doi.org/10.1016/j.ijbiomac.2020.03.231>

515 M. O. Adebajo, R. L. Frost, J. T. Klopogge, O. Carmody, S. Kokot (2003) Porous materials for oil spill
516 cleanup: A review of synthesis and absorbing properties. *J Porous Mat* 10: 159-170.
517 <https://doi.org/10.1023/A:1027484117065>

518 X. Long, X. B. Wei, Y. H. Qiu, M. Jiang, Z. Chen, Y. C. Song, . . . J. X. Liao (2021) Lead zirconate
519 titanate aerogel piezoelectric composite designed with a biomimetic shell structure for underwater
520 acoustic transducers. *Chem Commun* 57: 9764-9767. <https://doi.org/10.1039/d1cc03037j>

521 J. W. Long, A. E. Fischer, T. M. McEvoy, M. E. Bourg, J. C. Lytle, D. R. Rolison (2008) PMSE 430-Self-
522 limiting electropolymerization en route to ultrathin, conformal polymer coatings for energy-storage
523 applications. *Abstracts of Papers of the American Chemical Society* 236.

524 Q. Y. Zheng, Y. Tian, F. Y. Ye, Y. Zhou, G. H. Zhao (2020) Fabrication and application of starch-based
525 aerogel: Technical strategies. *Trends Food Sci Tech* 99: 608-620.
526 <https://doi.org/10.1016/j.tifs.2020.03.038>

527 H. B. Chen, P. Shen, M. J. Chen, H. B. Zhao, D. A. Schiraldi (2016) Highly Efficient Flame Retardant
528 Polyurethane Foam with Alginate/Clay Aerogel Coating. *Acs Appl Mater Inter* 8: 32557-32564.
529 <https://doi.org/10.1021/acsami.6b11659>

530 D. L. Plata, Y. J. Briones, R. L. Wolfe, M. K. Carroll, S. D. Bakrania, S. G. Mandel, A. M. Anderson
531 (2004) Aerogel-platform optical sensors for oxygen gas. *J Non-Cryst Solids* 350: 326-335.
532 <https://doi.org/10.1016/j.jnoncrysol.2004.06.046>

533 I. Smirnova, S. Suttiruengwong, W. Arlt (2004) Feasibility study of hydrophilic and hydrophobic silica
534 aerogels as drug delivery systems. *J Non-Cryst Solids* 350: 54-60.
535 <https://doi.org/10.1016/j.jnoncrysol.2004.06.031>

536 Z. Ulker, C. Erkey (2014) An emerging platform for drug delivery: Aerogel based systems. *J Control*

537 Release 177: 51-63. <https://doi.org/10.1016/j.jconrel.2013.12.033>

538 G. H. Yan, B. L. Chen, X. H. Zeng, Y. Sun, X. Tang, L. Lin (2020) Recent advances on sustainable
539 cellulosic materials for pharmaceutical carrier applications. *Carbohydr Polym* 244.
540 <https://doi.org/10.1016/j.carbpol.2020.116492>

541 L. Z. Zuo, Y. F. Zhang, L. S. Zhang, Y. E. Miao, W. Fan, T. X. Liu (2015) Polymer/Carbon-Based Hybrid
542 Aerogels: Preparation, Properties and Applications. *Materials* 8: 6806-6848.
543 <https://doi.org/10.3390/ma8105343>

544 H. Maleki (2016) Recent advances in aerogels for environmental remediation applications: A review.
545 *Chem Eng J* 300: 98-118. <https://doi.org/10.1016/j.cej.2016.04.098>

546 J. Estella, J. C. Echeverria, M. Laguna, J. J. Garrido (2007) Effects of aging and drying conditions on the
547 structural and textural properties of silica gels. *Micropor Mesopor Mat* 102: 274-282.
548 <https://doi.org/10.1016/j.micromeso.2007.01.007>

549 Y. Fu, Z. Guo (2022) Natural polysaccharide-based aerogels and their applications in oil–water
550 separations: a review. *J Mater Chem A* 10: 8129-8158. <https://doi.org/10.1039/d2ta00708h>

551 C. Alvarez-Lorenzo, B. Blanco-Fernandez, A. M. Puga, A. Concheiro (2013) Crosslinked ionic
552 polysaccharides for stimuli-sensitive drug delivery. *Adv Drug Deliver Rev* 65: 1148-1171.
553 <https://doi.org/10.1016/j.addr.2013.04.016>

554 M. Reches, E. Gazit (2003) Casting metal nanowires within discrete self-assembled peptide nanotubes.
555 *Science* 300: 625-627. <https://doi.org/10.1126/science.1082387>

556 A. Autissier, C. Le Visage, C. Pouzet, F. Chaubet, D. Letourneur (2010) Fabrication of porous
557 polysaccharide-based scaffolds using a combined freeze-drying/cross-linking process. *Acta Biomater* 6:
558 3640-8. <https://doi.org/10.1016/j.actbio.2010.03.004>

559 N. Benbettaieb, J. P. Gay, T. Karbowiak, F. Debeaufort (2016) Tuning the Functional Properties of
560 Polysaccharide-Protein Bio-Based Edible Films by Chemical, Enzymatic, and Physical Cross-Linking.
561 *Compr Rev Food Sci F* 15: 739-752. <https://doi.org/10.1111/1541-4337.12210>

562 H. J. Jing, X. Huang, X. J. Du, L. Mo, C. Y. Ma, H. X. Wang (2022) Facile synthesis of pH-responsive
563 sodium alginate/carboxymethyl chitosan hydrogel beads promoted by hydrogen bond. *Carbohyd Polym*
564 278. <https://doi.org/10.1016/j.carbpol.2021.118993>

565 C. Gao, X. L. Wang, Q. D. An, Z. Y. Xiao, S. R. Zhai (2021) Synergistic preparation of modified alginate
566 aerogel with melamine/chitosan for efficiently selective adsorption of lead ions. *Carbohyd Polym* 256.
567 <https://doi.org/10.1016/j.carbpol.2020.117564>

568 S. I. Jeong, M. D. Krebs, C. A. Bonino, S. A. Khan, E. Alsberg (2010) Electrospun Alginate Nanofibers
569 with Controlled Cell Adhesion for Tissue Engineering. *Macromol Biosci* 10: 934-943.
570 <https://doi.org/10.1002/mabi.201000046>

571 C. B. Tan, B. M. Fung, J. K. Newman, C. Vu (2001) Organic aerogels with very high impact strength.
572 *Adv Mater* 13: 644-646. [https://doi.org/10.1002/1521-4095\(200105\)13:9<644::AID-ADMA644>3.0.CO;2-#](https://doi.org/10.1002/1521-4095(200105)13:9<644::AID-ADMA644>3.0.CO;2-#)

573

574 R. J. Lin, A. Li, L. B. Lu, Y. Cao (2016) Preparation of bulk sodium carboxymethyl cellulose aerogels
575 with tunable morphology (vol 118, pg 126, 2015). *Carbohyd Polym* 151: 1278-1278.
576 <https://doi.org/10.1016/j.carbpol.2016.05.071>

577 H. R. Nie, M. Z. Liu, F. L. Zhan, M. Y. Guo (2004) Factors on the preparation of carboxymethylcellulose
578 hydrogel and its degradation behavior in soil. *Carbohyd Polym* 58: 185-189.
579 <https://doi.org/10.1016/j.carbpol.2004.06.035>

580 L. Li, S. L. Xiang, S. Q. Cao, J. Y. Zhang, G. F. Ouyang, L. P. Chen, C. Y. Su (2013) A synthetic route to

581 ultralight hierarchically micro/mesoporous Al(III)-carboxylate metal-organic aerogels. *Nat Commun* 4.
582 <https://doi.org/10.1038/ncomms2757>

583 M. N. Nadagouda, R. S. Varma (2007) Synthesis of thermally stable carboxymethyl cellulose/metal
584 biodegradable nanocomposites for potential biological applications. *Biomacromolecules* 8: 2762-2767.
585 <https://doi.org/10.1021/bm700446p>

586 S. H. Li, J. Y. Huang, Z. Chen, G. Q. Chen, Y. K. Lai (2017) A review on special wettability textiles:
587 theoretical models, fabrication technologies and multifunctional applications. *J Mater Chem A* 5: 31-55.
588 <https://doi.org/10.1039/c6ta07984a>

589 S. Wang, L. Jiang (2007) Definition of superhydrophobic states. *Adv Mater* 19: 3423-3424.
590 <https://doi.org/10.1002/adma.200700934>

591 J. D. Feng, S. T. Nguyen, Z. Fan, H. M. Duong (2015) Advanced fabrication and oil absorption properties
592 of super-hydrophobic recycled cellulose aerogels. *Chem Eng J* 270: 168-175.
593 <https://doi.org/10.1016/j.cej.2015.02.034>

594 K. Tsougeni, A. Tserepi, G. Boulousis, V. Constantoudis, E. Gogolides (2007) Control of nanotexture and
595 wetting properties of polydimethylsiloxane from very hydrophobic to super-hydrophobic by plasma
596 processing. *Plasma Processes Polym* 4: 398-405. <https://doi.org/10.1002/ppap.200600185>

597 N. T. Cervin, C. Aulin, P. T. Larsson, L. Wagberg (2012) Ultra porous nanocellulose aerogels as
598 separation medium for mixtures of oil/water liquids. *Cellulose* 19: 401-410.
599 <https://doi.org/10.1007/s10570-011-9629-5>

600 J. L. Xiao, W. Y. Lv, Y. H. Song, Q. Zheng (2018) Graphene/nanofiber aerogels: Performance regulation
601 towards multiple applications in dye adsorption and oil/water separation. *Chem Eng J* 338: 202-210.
602 <https://doi.org/10.1016/j.cej.2017.12.156>

603 Y. S. Yang, X. P. Chen, Y. M. Li, Z. C. Yin, M. T. Bao (2021) Construction of a Superhydrophobic Sodium
604 Alginate Aerogel for Efficient Oil Absorption and Emulsion Separation. *Langmuir* 37: 882-893.
605 <https://doi.org/10.1021/acs.langmuir.0c03229>

606 N. Kannan, M. M. Sundaram (2001) Kinetics and mechanism of removal of methylene blue by adsorption
607 on various carbons - a comparative study. *Dyes Pigments* 51: 25-40. [https://doi.org/10.1016/S0143-](https://doi.org/10.1016/S0143-7208(01)00056-0)
608 [7208\(01\)00056-0](https://doi.org/10.1016/S0143-7208(01)00056-0)

609 T. G. Mayerhofer, S. Pahlow, J. Popp (2020) The Bouguer-Beer-Lambert Law: Shining Light on the
610 Obscure. *Chemphyschem* 21: 2029-2046. <https://doi.org/10.1002/cphc.202000464>

611 V. Vimonses, S. M. Lei, B. Jin, C. W. K. Chowd, C. Saint (2009) Kinetic study and equilibrium isotherm
612 analysis of Congo Red adsorption by clay materials. *Chem Eng J* 148: 354-364.
613 <https://doi.org/10.1016/j.cej.2008.09.009>

614 Y. S. Ho, G. McKay (1999) Pseudo-second order model for sorption processes. *Process Biochem* 34:
615 451-465. [https://doi.org/10.1016/S0032-9592\(98\)00112-5](https://doi.org/10.1016/S0032-9592(98)00112-5)

616 C. Jiao, J. Xiong, J. Tao, S. Xu, D. Zhang, H. Lin, Y. Chen (2016) Sodium alginate/graphene oxide aerogel
617 with enhanced strength-toughness and its heavy metal adsorption study. *Int J Biol Macromol* 83: 133-41.
618 <https://doi.org/10.1016/j.ijbiomac.2015.11.061>

619 C. S. Robb, S. E. Geldart, J. A. Seelenbinder, P. R. Brown (2002) Analysis of green tea constituents by
620 HPLC-FTIR. *J Liq Chromatogr R T* 25: 787-801. <https://doi.org/10.1081/Jlc-120003036>

621 S. K. Zhou, T. T. You, X. M. Zhang, F. Xu (2018) Superhydrophobic Cellulose Nanofiber-Assembled
622 Aerogels for Highly Efficient Water-in-Oil Emulsions Separation. *ACS Appl Nano Mater* 1: 2095-2103.
623 <https://doi.org/10.1021/acsanm.8b00079>

624 S. K. Zhou, M. Wang, X. Chen, F. Xu (2015) Facile Template Synthesis of Microfibrillated

625 Cellulose/Polypyrrole/Silver Nanoparticles Hybrid Aerogels with Electrical Conductive and Pressure
626 Responsive Properties. *Acs Sustain Chem Eng* 3: 3346-3354.
627 <https://doi.org/10.1021/acssuschemeng.5b01020>

628 N. Abhari, A. Madadlou, A. Dini (2017) Structure of starch aerogel as affected by crosslinking and
629 feasibility assessment of the aerogel for an anti-fungal volatile release. *Food Chem.* 221: 147-152.
630 <https://doi.org/10.1016/j.foodchem.2016.10.072>

631 C. Y. Chang, B. Duan, L. N. Zhang (2009) Fabrication and characterization of novel macroporous
632 cellulose-alginate hydrogels. *Polymer* 50: 5467-5473. <https://doi.org/10.1016/j.polymer.2009.06.001>

633 C. X. Liang, K. Hirabayashi (1992) Improvements of the Physical-Properties of Fibroin Membranes with
634 Sodium Alginate. *J Appl Polym Sci* 45: 1937-1943. <https://doi.org/10.1002/app.1992.070451108>

635 F. C. Wu, R. L. Tseng, R. S. Juang (2009) Initial behavior of intraparticle diffusion model used in the
636 description of adsorption kinetics. *Chem Eng J* 153: 1-8. <https://doi.org/10.1016/j.cej.2009.04.042>

637

Supplementary Files

This is a list of supplementary files associated with this preprint. Click to download.

- [SupportInformation.docx](#)
- [Graphicabstract.tif](#)